Appl. No. 10/874,110 Amdt. dated November 20, 2006 Amendment under 37 CFR 1.116 Expedited Procedure Examining Group 2617

Amendments to the Specification:

Please replace the paragraph which begins on line 14 of page 10 with the following amended paragraph:

Main refrigerant is removed from the outlet 30 of the cold side 29 of the liquefaction heat exchanger 5, connected through conduit 53 to inlet 51 of the turbine-driven liquefaction compressor 50, where it is compressed to an elevated pressure. The heat of compression is removed in cooler 56 and further heat is removed from the main refrigerant in the refrigerant heat exchanger 58 to obtain partly condensed refrigerant. Partly condensed main refrigerant is then separated in separator 60 into a heavy, liquid fraction and a light, gaseous fraction, which fractions are further cooled in the second and the third hot side sides 67 and 77 respectively to obtain liquefied and sub-cooled fractions at elevated pressure. The sub-cooled refrigerants are then allowed to expand in expansion devices 70 and 80 to a lower pressure. At this pressure the refrigerant is allowed to evaporate in the cold side 29 of the liquefaction heat exchanger 5 to remove heat from the natural gas passing through the first cold side 25.

Please replace the paragraph which begins on line 30 of page 11 with the following amended paragraph:

Instead of turbines, electric motors can be used to drive the compressors 31, 50 and 131 in the pre-cooling refrigerant circuit. 3 and the main refrigerant circuit 9, and the **additional** pre-cooling refrigerant circuit 43.

Please replace the paragraph which begins on line 8 of page 13 with the following amended paragraph:

In the embodiment of FIG. 2, each main refrigerant circuit 9 and 9' comprises a complete <u>additional</u> pre-cooling circuit 43 and 43', where each <u>additional</u> pre-cooling circuit is identical to the one disclosed in FIG. 1.

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Please replace the paragraph which begins on line 28 of page 13 with the following amended paragraph:

Reference is now made to FIG. 4, which shows schematically an alternative of the additional pre-cooling refrigerant circuits 43 and 43' as shown in FIG. 3. The refrigerant heat exchangers 58 and 58' shown in FIG. 3 are combined in one integrated heat exchanger 202. The integrated heat exchanger 202 has a cold side 215 in which are arranged the hot sides 57 and 57' pertaining to the main refrigerant circuits 9 and 9', respectively. In this embodiment, the pre-cooling refrigerant is suitably a multi-component refrigerant comprising nitrogen, methane, ethane, propane and butane. During normal operation, evaporated pre-cooling refrigerant is removed from the cold side 215 through conduit 241, compressed to an elevated pressure by the precooling refrigerant compressor 231 (having an inlet 233 and an outlet 234), cooled in cooler 236 through conduit 235 and supplied to additional hot side 243 arranged in the cold side of the integrated heat exchanger 202. In the additional hot side 243, the pre-cooling refrigerant is liquefied against evaporating refrigerant. The liquefied pre-cooling refrigerant is removed from the additional hot side 243 through conduit 245 provided with expansion device in the form of throttle 246, where it is allowed to expand to a lower pressure. At this lower pressure the refrigerant is supplied through injection nozzle 248 into the inlet of the cold side 215.